

موضوع الامتحان لمصر، صفحات ١١٠ (١)

الفرم الثاني من كتابنا قوس

٢٠١٦ - ٢٠١٨

ترم اول

دكتوراه في الفقه

Q<sub>1</sub> [15]

- 1) ✓
- 2) X increases
- 3) X 0 %
- 4) X 165 bar
- 5) X non identical
- 6) X Feed water or IM superheater
- 7) X Simple gas turbines cycle or without or wet suite
- 8) X decreases
- 9) ✓
- 10) X stay constant or velocity decreases
- 11) ✓
- 12) X inCondenser

Q2 [15 Marks]

Given:-  $P_1 = 28 \text{ bar}$        $T_1 = 400^\circ\text{C}$        $P_c = 0.03332 \text{ bar}$

$X_4 = 90\%$

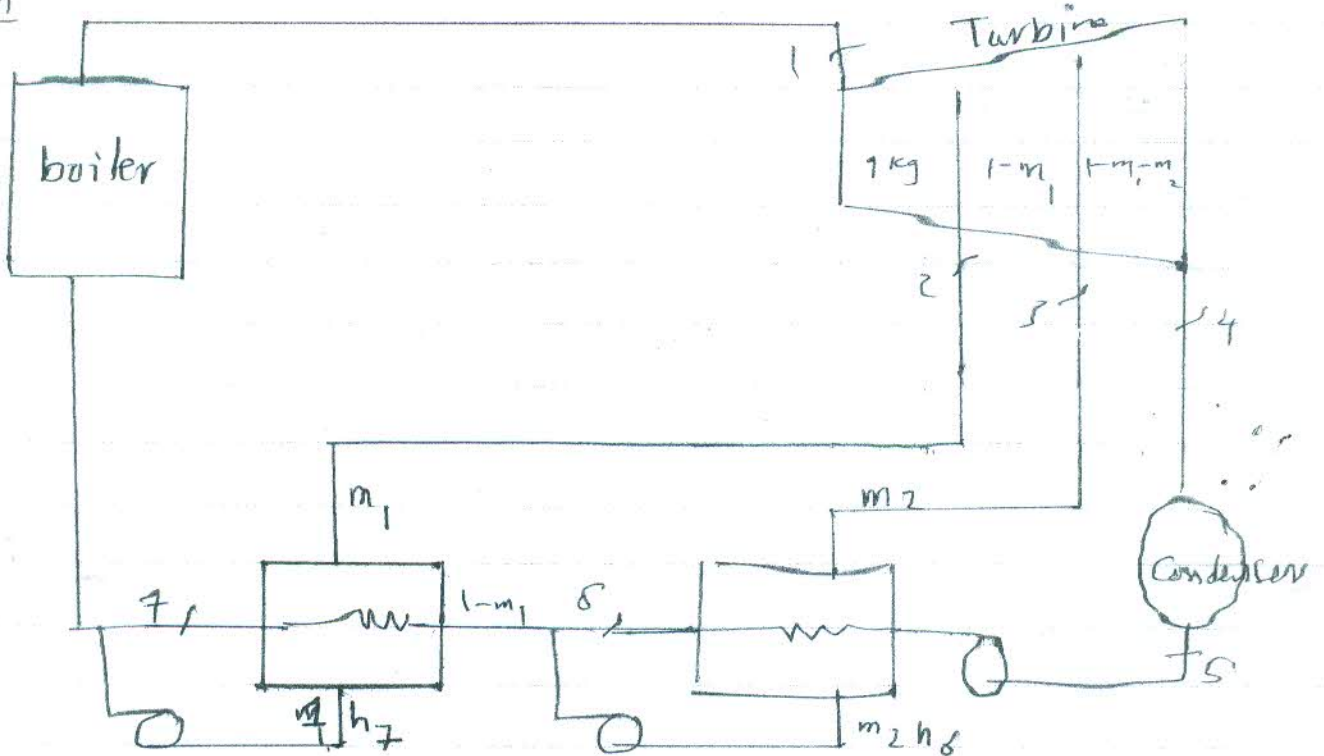
$$h_1 - h_2 = h_2 - h_3 = h_3 - h_4$$

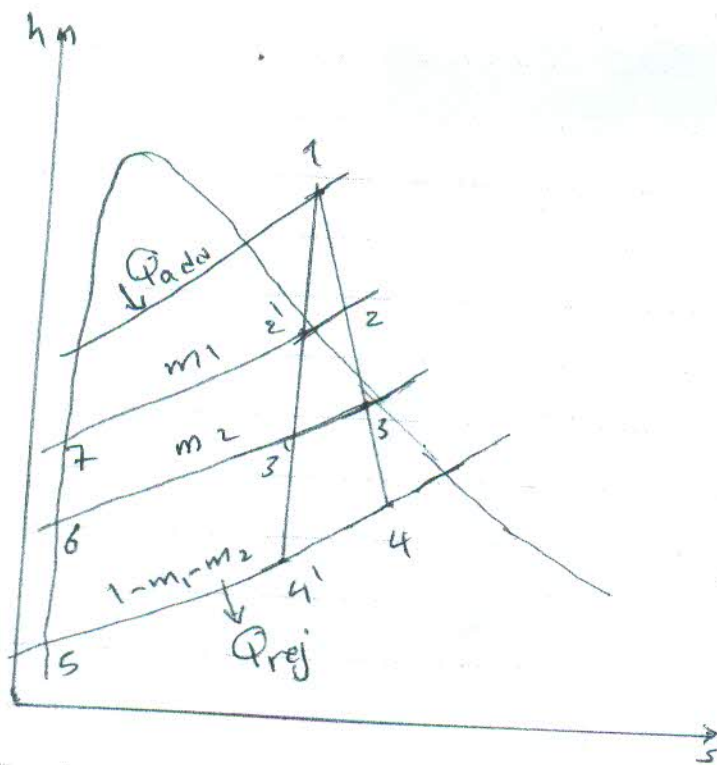
Req:- a) The bleeding pressures

b)  $\eta_m$

c)  $\eta_t$

Soln





( at  $P_1 = 28 \text{ bar}$        $T_1 = 400^\circ\text{C}$        $h_1 = 3235 \text{ kJ/kg}$

at  $P_4 = P_c = 0.0332 \text{ bar}$        $x_4 = 0.9$        $h_4 = 2310 \text{ kJ/kg}$

$$\frac{h_1 - h_4}{3} = \frac{3235 - 2310}{3} = 308.4 \text{ kJ/kg}$$

$h_1 - h_2 = 308.4$        $h_2 = 2926.6 \text{ kJ/kg}$

$h_2 - h_3 = 308.4$        $h_3 = 2618.2 \text{ kJ/kg}$

$P_2$  at  $h_2 = 2926.6$        $P_2 = 5 \text{ bar}$

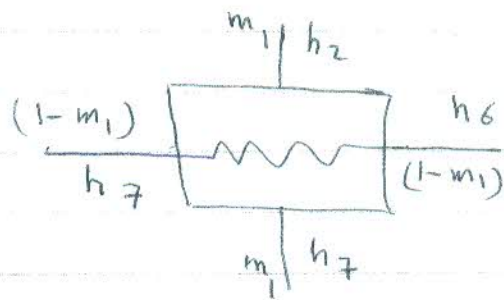
$P_3$  at  $h_3 = 2618.2$        $P_3 = 0.55 \text{ bar}$

$P_5 = 0.03332 \text{ bar at sat}$        $h_5 = \frac{121.4 + 73.5}{2} \approx 100 \text{ kJ/kg}$

$P_6 = 0.55 \text{ bar at sat}$        $h_6 = 350.6 \text{ kJ/kg}$

$P_7 = 5 \text{ bar at sat}$        $h_7 = 640.1 \text{ kJ/kg}$

Heat balance of Feed water heater (I)



$$m_1 h_2 + (1 - m_1) h_6$$

$$= m_1 h_7 + (1 - m_1) h_7$$

$$m_1 = \frac{h_7 - h_6}{(h_2 - h_7) + (h_7 - h_6)} = \frac{640.1 - 350.6}{2926.6 - 350.6} = 0.1124 \frac{\text{kg}_{\text{st}}}{\text{kg}_{\text{st}}}$$

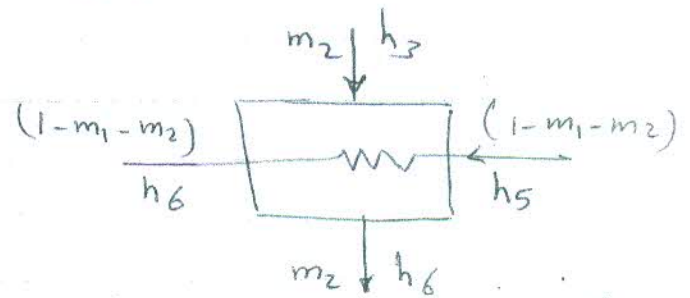
Heat balance of Feedwater heater (II)

$$m_2 h_3 + (1 - m_1 - m_2) h_5$$

$$= m_2 h_6 + (1 - m_1 - m_2) h_6$$

$$m_2 h_2 = \frac{(1 - m_1) h_6 - (1 - m_1) h_6}{h_3 - h_5}$$

$$= \frac{(1 - 0.1124)(350.6 - 100)}{2618.2 - 100} = 0.0883 \frac{\text{kg}_{\text{st}}}{\text{kg}_{\text{st}}}$$



$$\eta_{\text{th}} = \frac{(h_1 - h_2) + (1 - m_1)(h_2 - h_3) + (1 - m_1 - m_2)(h_3 - h_4)}{h_1 - h_2}$$

$$= \frac{308.4 [1 + 1 - 0.1124 + 1 - 0.1124 - 0.0883]}{3235 - 640.1} = 32\%$$

$$\eta_c = \frac{h_1 - h_4}{h_1 - h_{4s}} = \frac{3235 - 2310}{3235 - 2075} = 80\%$$

$h_{4s}$  at  $s_1 = s_{4s}$   $h_{4s} = 2075 \text{ kJ/kg}$

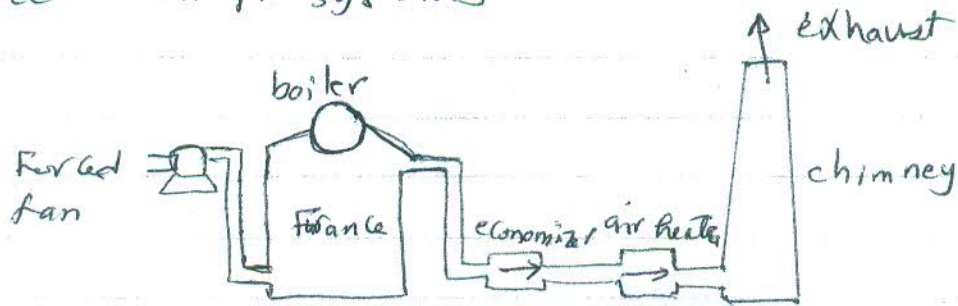
Q3 [9] [25 marks]

Large steam generators require an assist to push the air in, pull the

the gas out, or both. The basic types of mechanical systems are

a) Forced-draft      b) induced draft      c) balanced draft

a) Forced-draft systems



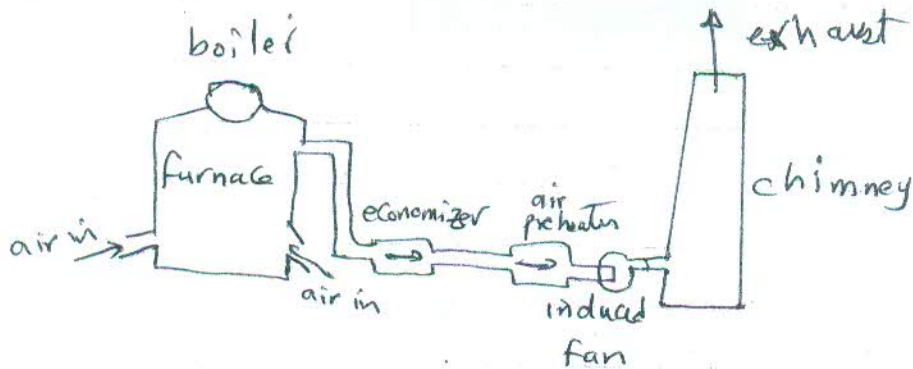
In the forced draft system, the fan placed at the air entrance to the air preheater. The forced fan pumps only cold, clean combustion air, and the resulting positive pressure in the combustion chamber improves the gas side convection coefficient.

$$m_{f.d} = m_f \left( \frac{A}{F} \right) \text{ or}$$

$$m_{f.d} = m_f (1+W) \left( \frac{A}{F} \right)$$

There are two types of fans in common use centrifugal and axial.

b) induced-draft systems



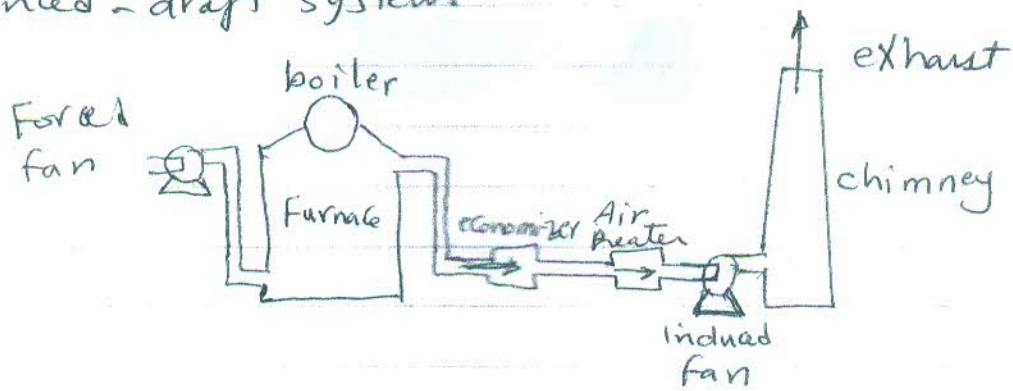
In induced-draft system the fan is located in the gas stream between the air preheater and the stack. It draws combustion products from the combustion chamber and discharges them into the stack. This produces a negative pressure in the combustion chamber, eliminating the leakage problem.

$$\dot{m}_{i-d} = \dot{m}_f \left[ \left( \frac{A}{F} \right) + 1 - R \right] \quad \text{or}$$

$$\dot{m}_{i-d} = \dot{m}_f \left[ \left( \frac{A}{F} \right) (1+w) + 1 - R \right]$$



### (c) balanced-draft systems



balanced-draft system employs both forced draft and induced draft fan. In this system, the combustion chamber operates at or slightly below atmospheric pressure. The forced fan push air through the air preheater, dampers, various air ducts, and burners into furnace. The induced fan pull the combustion gases from the furnace to stack.

\* The advantages of forced draft over the induced draft are

1 - They have lower maintenance problems.

2 - They consume much less power.

3 - Their capital and operating costs are lower.

4 - Their load is reduced by the absence of fuel added.

(Q3) [b]

$$\eta_{\text{mp}} = \frac{\text{Power}}{\dot{m}_f \cdot HV} = \frac{300 \times 10^3}{\dot{m}_f \times 44000} = 0.35$$

$$\dot{m}_f = \frac{300 \times 10^3}{(1 - 0.14 - 0.11) \times 0.35 \times 44000} = \frac{300 \times 10^3}{11550} = 25.974$$

$$\eta_{\text{mc}} = \frac{\text{Power}}{\dot{Q}_{\text{add}}} \Rightarrow \dot{Q}_{\text{add}} = \frac{300 \times 10^3}{0.43} = 697674.418$$

$$\dot{Q}_f = \frac{\dot{Q}_{\text{add}}}{\dot{m}_f} = \frac{697674.418}{25.974} = 26866.49 \text{ kg/kg}_f$$

$$\dot{Q}_f = \dot{m}_f \cdot HV = (1 - 0.14 - 0.11) \times 44000 = 33000 \text{ kg/kg}_f$$

$$N_2 \% = 100 - 13.78 - 4.49 - 0.75 = 80.98 \%$$

$$A/f = \frac{C \% \times N_2 \%}{33(CO \% + CO_2 \%)} = \frac{85(1 - 0.14 - 0.11) \times 80.98}{33(0.75 + 13.78)}$$

$$= 10.766 \text{ kg}_{\text{air}} / \text{kg}_f$$

$$\dot{m}_g = A/f + 1 - R - M - 9H_2$$

$$= 10.766 + 1 - 0.12 - 0.14 - 9(1 - 0.14 - 0.11) \times 0.057$$

$$= 11.12 \text{ kg}_g / \text{kg}_f$$

$$\dot{Q}_g = \dot{m}_g \varphi_g (T_{g0} - T_{gi}) = 11.12 \times 1.05 \times (288 - 50)$$

$$= 2779.765 \text{ kg/kg}_f$$

$$m_{S_1} = H + 9H_2 = 0.14 + 9 \times (1 - 0.14 - 0.11) \times 0.057$$

$$= 0.52475 \text{ kg}_w / \text{kg}_f$$

$$h_s - h_w = 2837.9$$

$$Q_{S_1} = m_{S_1} (h_s - h_w) = 0.52475 \times 2837.9 = 1489.188 \text{ kg/kg}$$

$$W = \frac{0.622 P_{\text{par}}}{P_{\text{at}} - P_{\text{par}}} = \frac{0.622 \times 0.0617}{0.942 - 0.0617} = 0.0436 \text{ kg}_{H_2O} / \text{kg}_{\text{air}}$$

$$Q_v = A/F W C_{p_w} (T_{g_0} - T_{g_i})$$

$$= 10.766 \times 0.0436 \times 1.926 \times (288 - 50)$$

$$= 215.166 \text{ kg/kg}_f$$

$$m_{CO} = \frac{C_b \times CO\%}{CO\% + CO_2\%} = \frac{(1 - 0.11 - 0.14) \times 0.85 \times 0.75}{0.75 + 13.78}$$

$$= 0.0304 \text{ kg/kg}_f$$

$$Q_{CO} = m_{CO} \times 23630 = 0.0304 \times 23630 = 777 \text{ kg/kg}_f$$

$$Q_{\text{unacc}} = Q_f - [Q_r + Q_g + Q_{S_1} + Q_v + Q_{CO}] = 878.879$$

Q<sub>4</sub> [10 Marks]

$$P_t = P_b - P_v = 764 - 680 = 84 \text{ mm Hg}$$

$$P_t = 0.084 \times 13600 \times 9.81 = 11.206 \text{ kPa}$$

$$P_t = P_s + P_a$$

$$P_s = P_{sat} \text{ at } t = 36.2 \quad P_s = 6.05 \text{ kPa}$$

$$P_a = P_t - P_s = 5.155 \text{ kPa}$$

$$\eta_v = \frac{P_{sat} - P_t}{P_{sat} - P_s} = \frac{101.928 - 11.206}{101.928 - 6.05} = 94.622\%$$

$$P_v = mRt$$

$$v = \frac{1.78 \times 287 \times (36.2 + 273)}{5.155 \times 10^3} = 30.641 \text{ m}^3$$

Q5 [10 marks]

Data:  $\alpha_1 = 20^\circ$

$c_1 = 375 \text{ m/s}$       $U = 165 \text{ m/s}$

$c_{f1} = c_{f2}$

$F_c = 0$

$k = 0.85$

$m_{st} = 1 \text{ kg/s}$

Req:

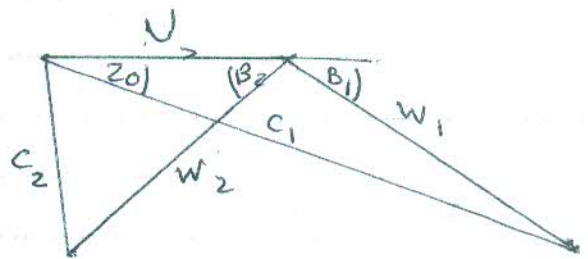
$B_1$ ,  $B_2$ , Power,  $m_{st} \frac{c_2^2}{2}$

Soln

Scale  $1 \text{ cm} = 50 \frac{\text{m}}{\text{s}}$

$U = \frac{165}{50} = 3.3 \text{ cm}$

$c_1 = \frac{375}{50} = 7.5 \text{ cm}$



$w_1 = 4.6 \text{ cm} = 230 \text{ m/s}$

$k = \frac{w_2}{w_1} = 0.85$

$w_2 = 0.85 w_1 = 195.9 \text{ m/s} = 3.91 \text{ cm}$

$B_1 = 35^\circ$

$B_2 = 41^\circ$

$w_c = 6.8 \text{ cm} = 340 \text{ m/s}$

Power =  $m_{st} \cdot w_c \cdot U = 1 \cdot 340 \cdot 165 = 56.1 \text{ kW}$

$c_2 = 2.65 \text{ cm} = 132.5 \text{ m/s}$

$m_{st} \cdot \frac{c_2^2}{2} = 1 \cdot \frac{132.5^2}{2} = 8778.125 \text{ J/s} = 8.778 \text{ kW}$